

Thermal Hydraulics of Supercritical Water Reactor (SCWR)

Prof. Xiaojing Liu

30 July 2025

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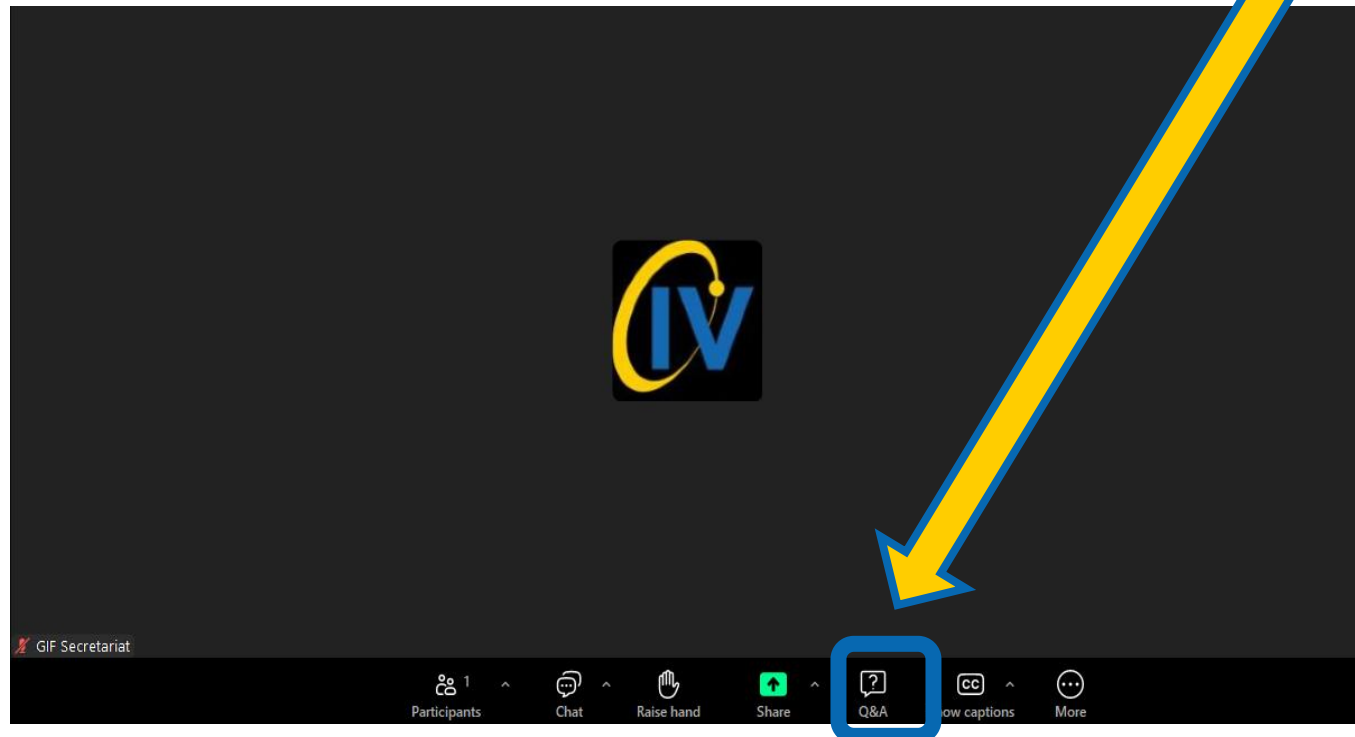
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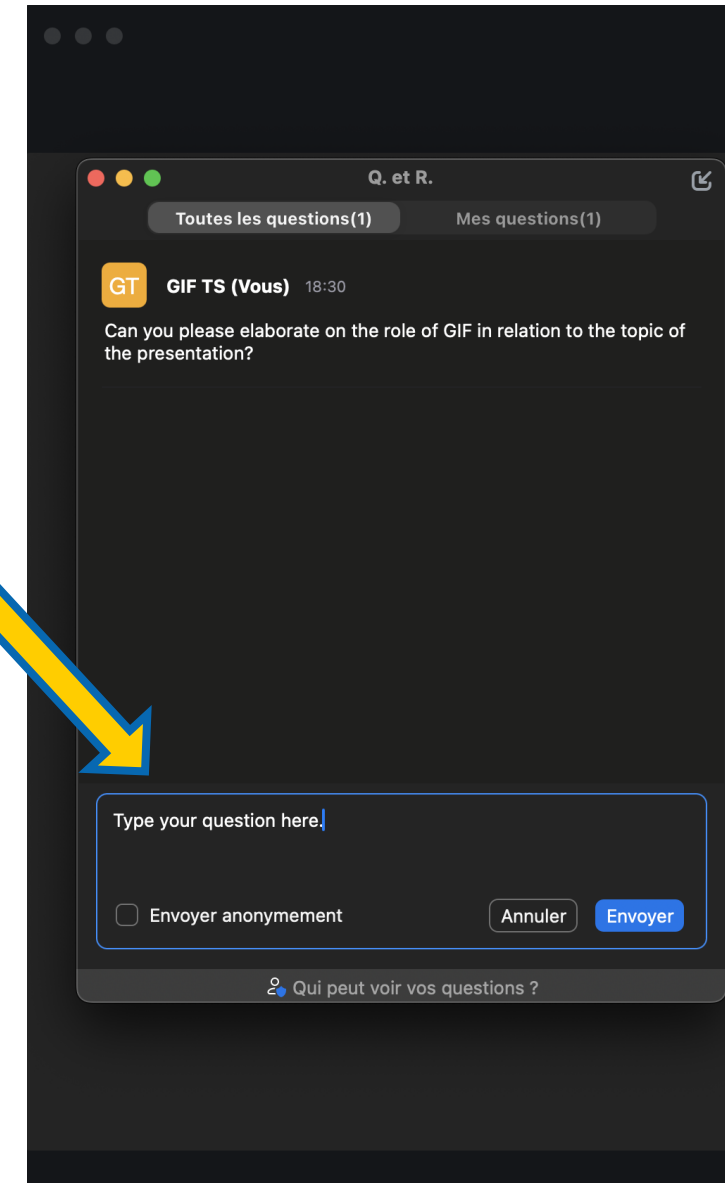
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上海交通大学
SHANGHAI JIAO TONG UNIVERSITY

Meet the Presenter

Professor **Xiaojing Liu** from Shanghai Jiao Tong University in China obtained his Ph.D. degree from SJTU in 2010. He was a postdoctoral fellow at the Karlsruhe Institute of Technology (KIT) in Germany from 2012 to 2013.

He is currently the director of the Shanghai integrating innovation center for digital reactors, leader of the Innovative Nuclear System Laboratory (INSL) in SJTU and has long been engaged in research on advanced and digital nuclear energy systems. He has published over 200 papers in renowned journals such as Applied Energy, Energy Conversion and Management, and Annals of Nuclear Energy.

He serves as a board member of the Nuclear Reactor Thermal-Hydraulics Division of the Chinese Nuclear Society, Associate editor of ASME Journal of Nuclear Engineering and Radiation Science (JNERS), Editorial Advisory Board member of Nuclear Engineering and Design, Youth editorial board member of Nuclear Science and Techniques and Frontiers in Energy.

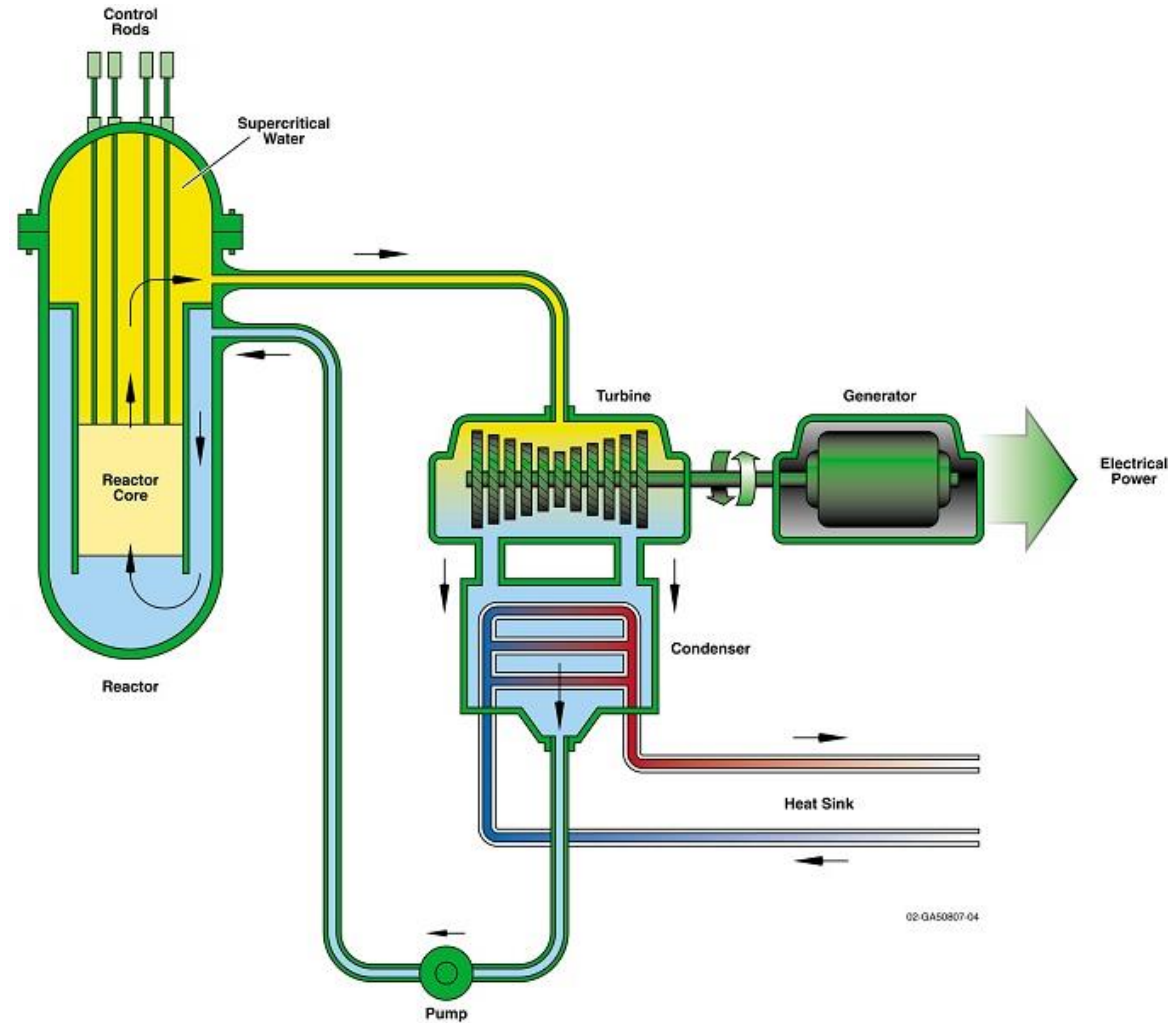


Introduction

Supercritical Water Cooled Reactor (SCWR)

P: 25MPa

T: 500°C



Introduction

- ✓ Simple & compact plant systems
- ✓ No water/steam separation
- ✓ Low flow rate(1/8-1/5), high enthalpy coolant
- ✓ High temperature & thermal efficiency (510 C, ~44%)
- ✓ Flexibility of the neutron spectrum, increase the utilization of the fuel
- ✓ Utilizations of current LWR and Supercritical FPP technologies
- ✓ Major components are used within the temperature range of past experiences

Introduction

Features	PWR	BWR	SCWR
System structure	Two loop	one loop	One loop
Flow path in core	Once through	Recirculation	Multi paths
Flow direction	Vertical upward	Vertical upward	Up- & downward
TH parameter	Sub-critical; sub-cooled	Sub-critical, high void fraction	Supercritical
Pressure	15-16 MPa	7 MPa	25 MPa
Temperature	290°C – 330°C	215°C – 285°C	280°C – 500°C
Mass flux	High	Medium	low
Geometry	Large FA	Small FA	both
Lattice	Square, wide		Semi-tight
Spacers	Grid	Grid	Grid & wire wrap
Moderator channel	No	yes	Co- & count current flow
Design criteria	Fuel temperature & CHF		Temperature

Introduction

- Extreme operating conditions
 - high pressure
 - high temperature
 - high heat flux
 - neutron irradiation



- Challenges in core/fuel assembly design
 - large property variation
 - non-uniformity of moderation
 - sensitive to hot channel factor
 - non-uniformity of local heat transfer
 - Blockage of the bundle
 - upper limit of cladding temperature

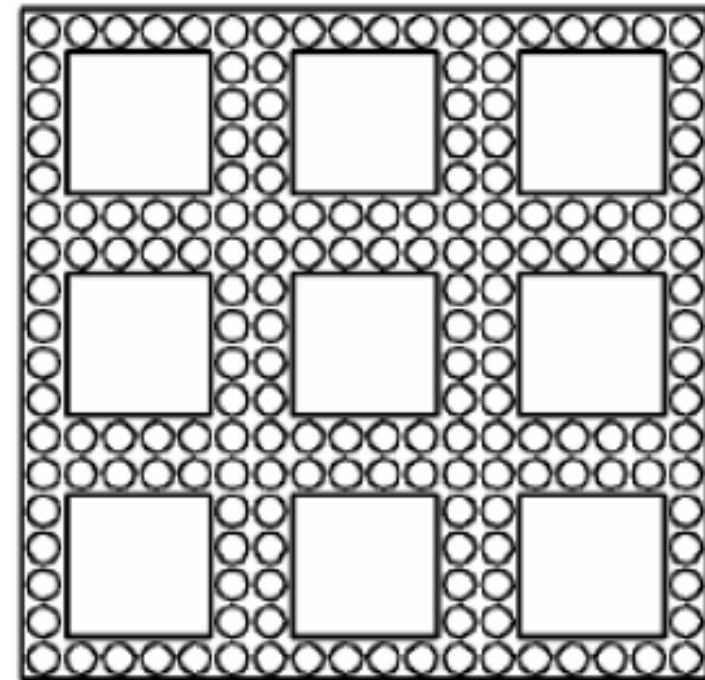
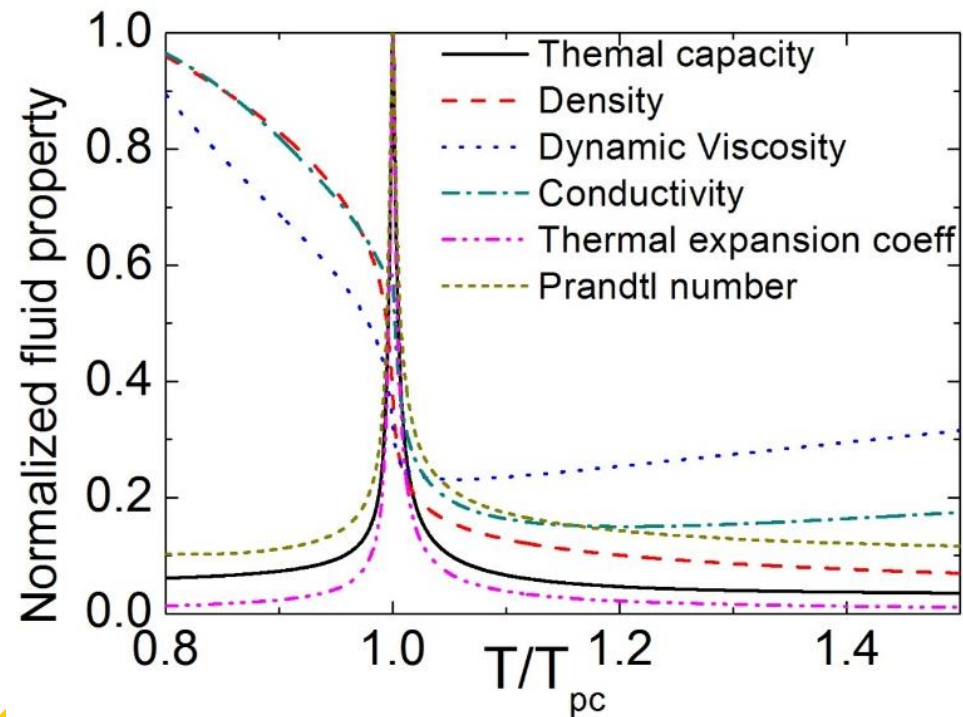


Introduction

Supercritical Water Cooled Reactor (SCWR)

P: 25MPa

T: 500°C



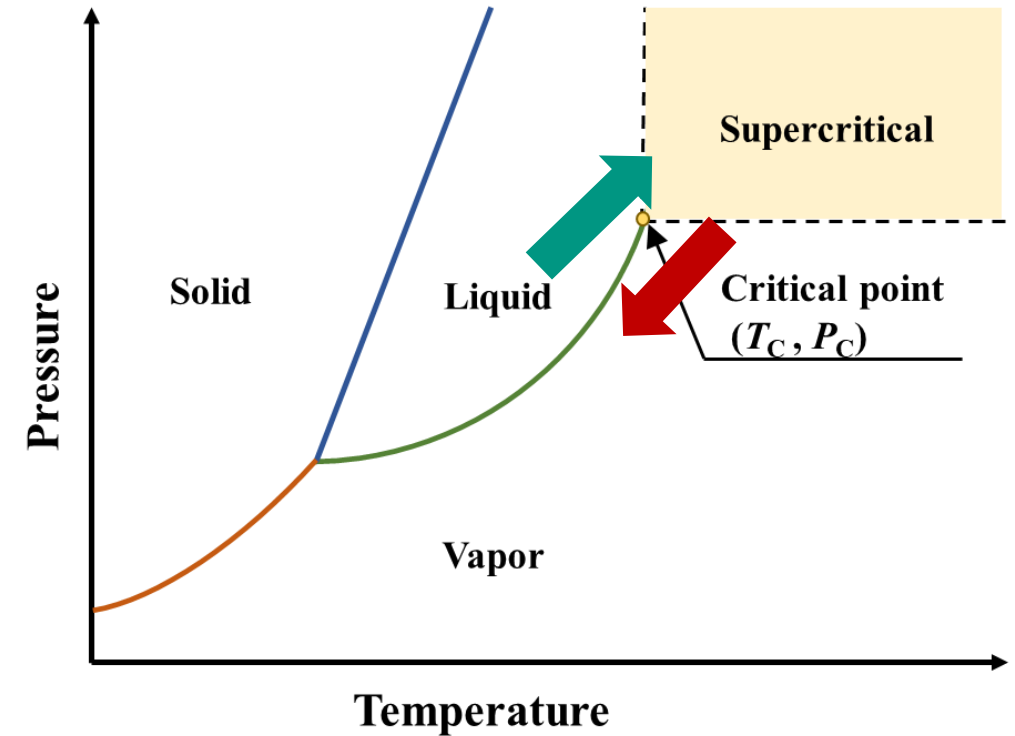
Supercritical Water Cooled Reactor (SCWR)

➤ Supercritical condition

- Single-phase
- No Boiling crisis

➤ Trans-critical transient

- Start-up
- Shut-down
- Accident



Contents

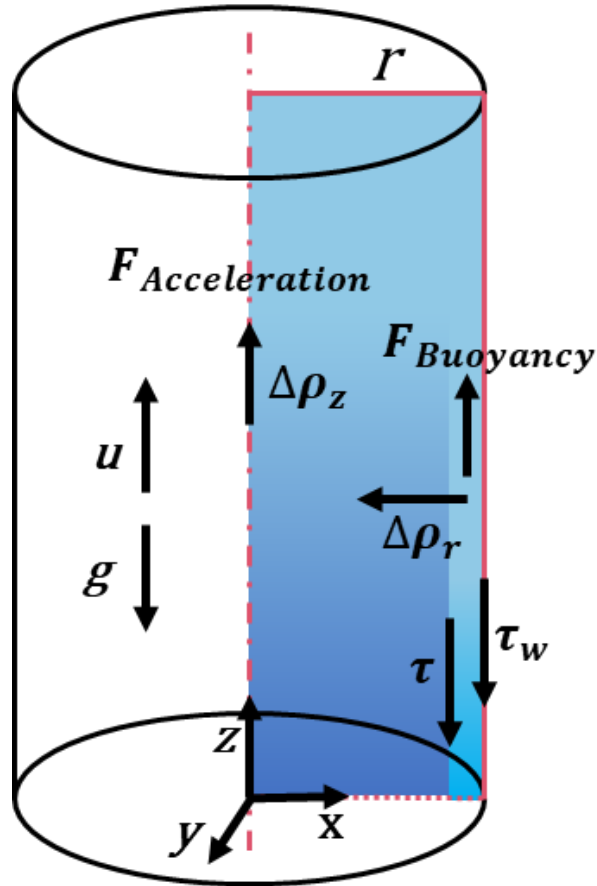
- 1. Introduction**
- 2. Heat transfer at Supercritical condition**
- 3. Heat transfer at Subcritical condition**
- 4. Heat transfer during Trans-critical transient**
- 5. Conclusions**

Supercritical condition

- **Heat transfer databank at supercritical condition**
 - **More than 90 000 data points**
 - **Supercritical H₂O : 31 516 data points**
 - **Supercritical R134a : 47 075 data points**
 - **Supercritical CO₂ : 21 113 data points**

Pressure (MPa)	Mass flux (kg/m ² s)	Heat flux (MW/m ²)	Tube diameter (mm)
22.3 - 41.0	100 - 3600	0.1 - 9.4	1.3 - 46.0

Supercritical condition



➤ **Acceleration effect: Main flow direction**

$$\pi_A \propto \frac{\partial \rho}{\partial z} \propto \frac{\beta q}{c_p G}$$

➤ **Buoyancy effect: Radial direction**

$$\pi_B \propto \frac{\partial \rho}{\partial y} \propto \frac{\beta D q}{\lambda} \propto \pi_A \cdot Re \cdot Pr$$

Supercritical condition

$$h = 0.023 \cdot Re^{0.8} \cdot Pr^{\frac{1}{3}} \cdot \frac{\lambda}{D} \cdot F_1 \cdot F_2$$

$$F_1 = \begin{cases} 0.98 & \pi_A < 1.75 \cdot 10^{-4} \\ 0.85 + 0.056 \cdot (10^4 \cdot \pi_A)^{1.5}, & 1.75 \cdot 10^{-4} < \pi_A < 3.75 \cdot 10^{-4} \\ \frac{13.2}{4.5 + (10^4 \cdot \pi_A)^{1.35}} & \pi_A > 3.75 \cdot 10^{-4} \end{cases}$$

$$F_2 = \begin{cases} 0.96 \cdot \left(\frac{Pr}{2.5}\right)^{0.265}, & Pr < 2.5 \\ 1.66 \cdot \left(\frac{Pr}{2.5}\right)^{-0.333}, & Pr > 2.5 \end{cases}$$

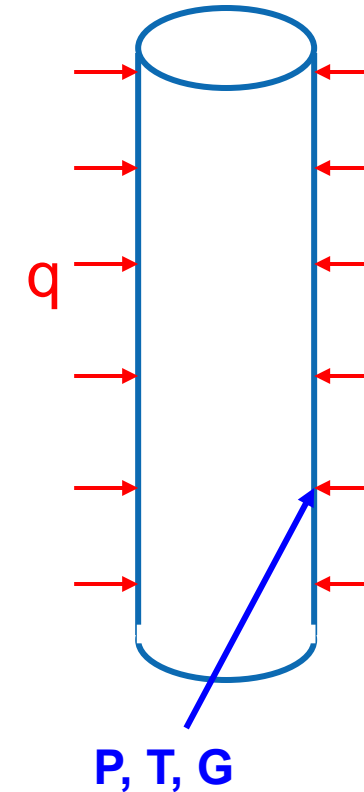
Supercritical condition

➤ Model validation

	Supercritical H ₂ O (N=23547)		Supercritical R134a (N=47075)		Supercritical CO ₂ (N= 21113)	
	μ	σ	μ	σ	μ	σ
Present Model	-0.008	0.163	0.035	0.163	0.135	0.247
Cheng correlation	-0.037	0.171	0.112	0.120	0.038	0.208
Bishop correlation	-0.082	0.103	-0.063	0.076	-0.058	0.132
Jackson correlation	-0.101	0.143	-0.005	0.096	-0.076	0.136

Scaling analysis

- **Object considered**
circular tubes, vertical oriented
uniformly heated
- **Parameter to be separately controlled are:**
tube diameter
heated length (*neglected for developed flow*)
pressure
fluid temperature
mass flux
heat flux
- **Parameter to be studied**
heat transfer coefficient, or
wall temperature



Scaling analysis

Required parameters in
prototypical fluid, water:

$$D_P, p_P, T_P, G_P, q_P$$



$$f_D = \frac{D_M}{D_P} = 1.0$$

$$f_P = \frac{P_M}{P_P} = \frac{P_{C,M}}{P_{C,P}}$$

$$f_\theta = \frac{\theta_{B,M}}{\theta_{B,P}} = 1.0$$

$$f_G = \frac{G_M}{G_P} = \frac{\text{Pr}_{B,P}^{5/12}}{\text{Pr}_{B,M}^{5/12}} \cdot \frac{\mu_{B,M}}{\mu_{B,P}}$$

$$f_q = \frac{q_M}{q_P} = \frac{\lambda_{B,M}(T_{PC} - T_C)_M}{\lambda_{B,P}(T_{PC} - T_C)_P}$$



Experimental parameters
in model fluid, e.g. CO₂:

$$D_M, p_M, T_M, G_M, q_M$$



Experimental results in
model fluid:

$$\alpha_P$$



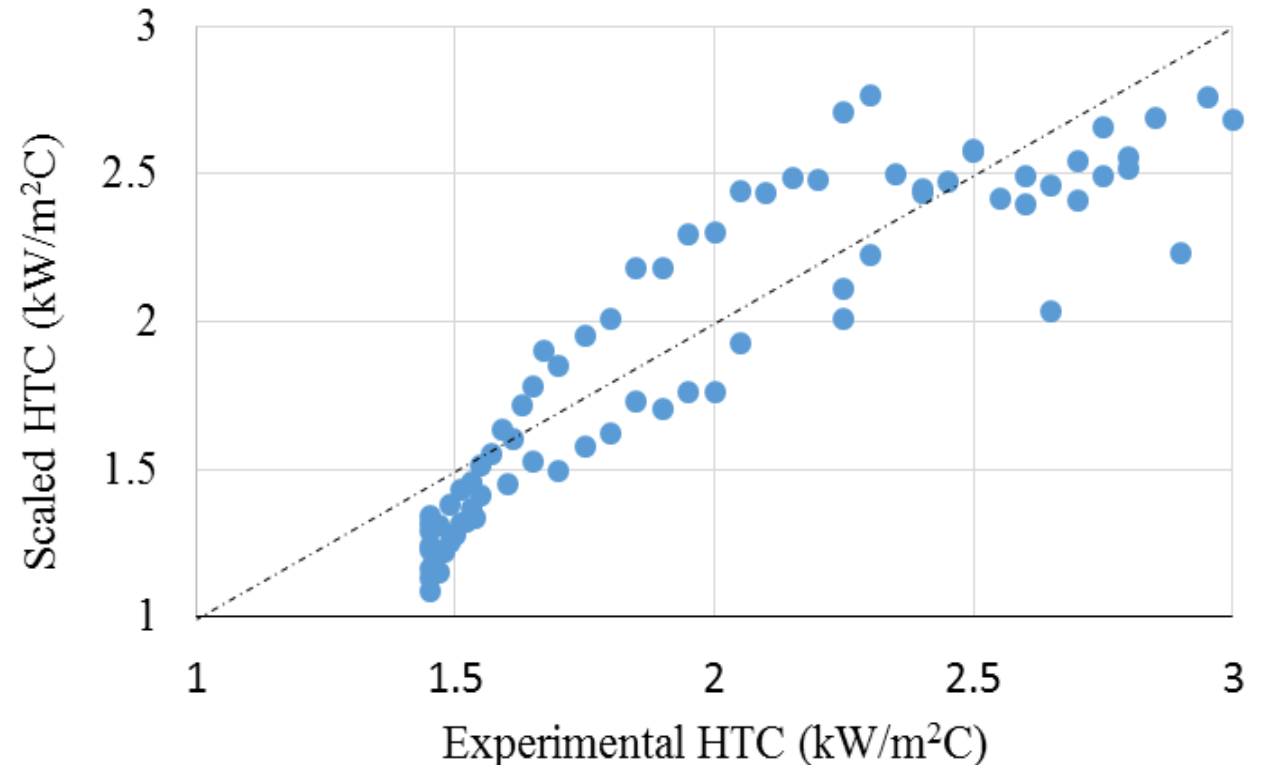
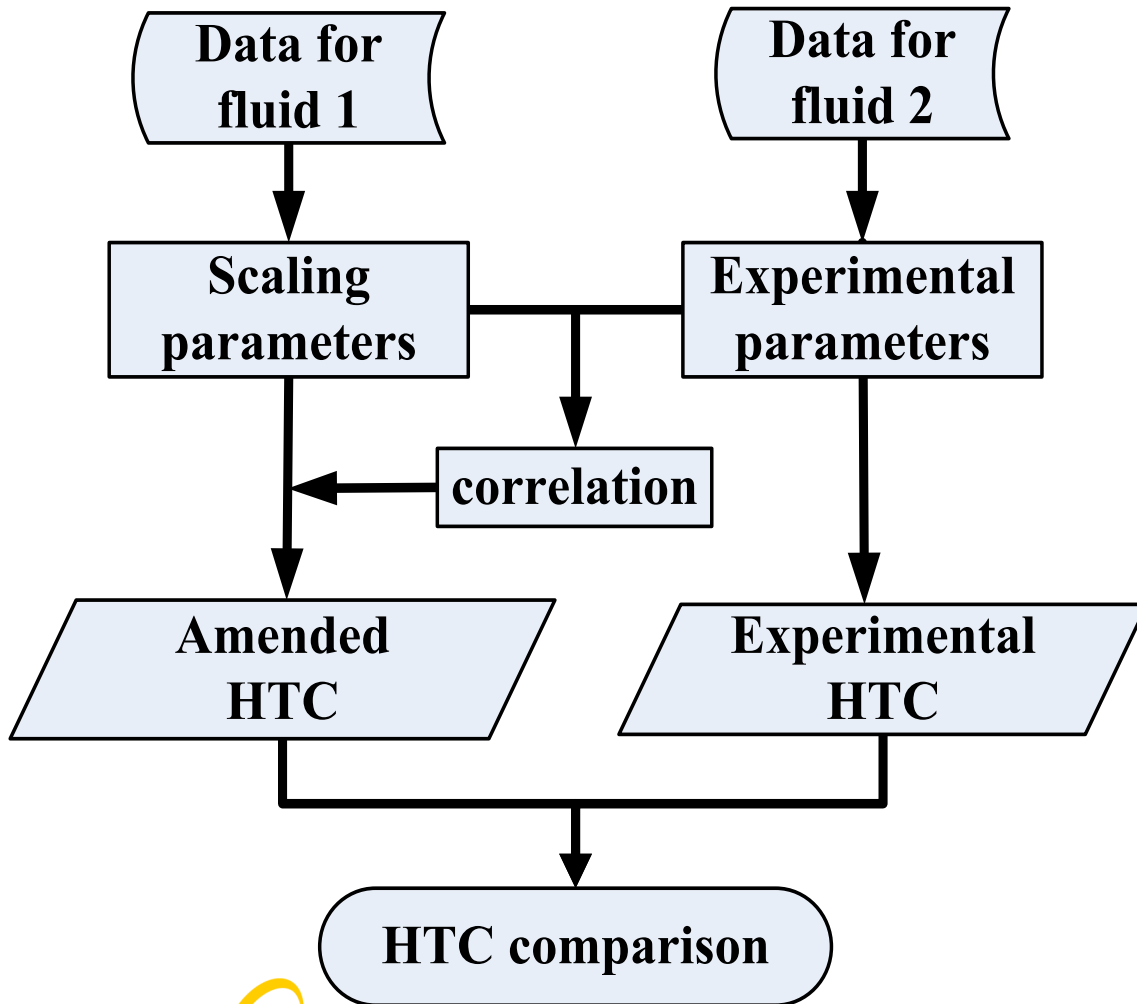
$$f_\alpha = \frac{\alpha_M}{\alpha_P} = \frac{\lambda_{B,M}}{\lambda_{B,P}}$$



Experimental results in
model fluid:

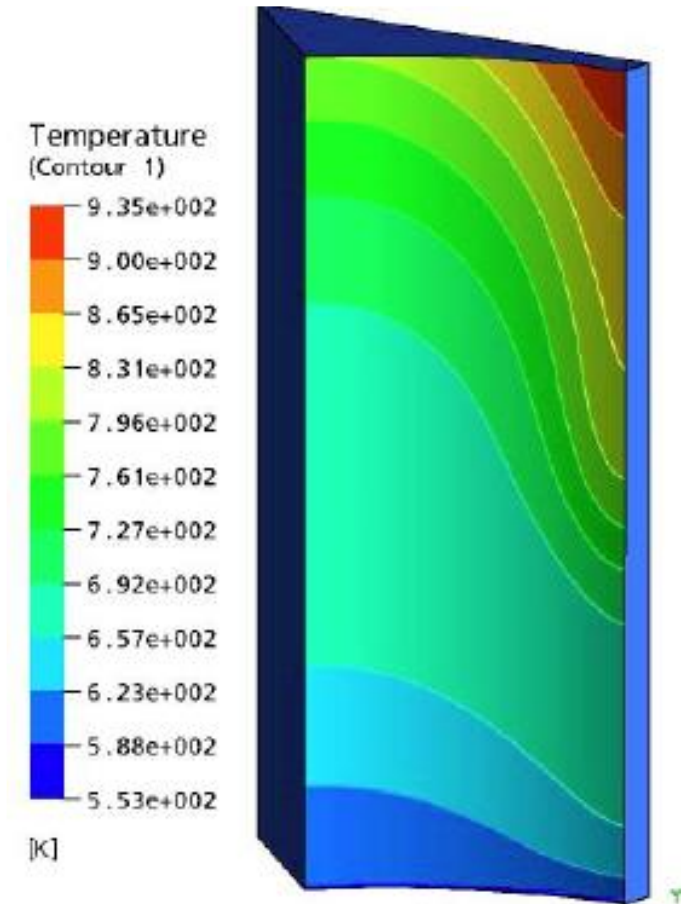
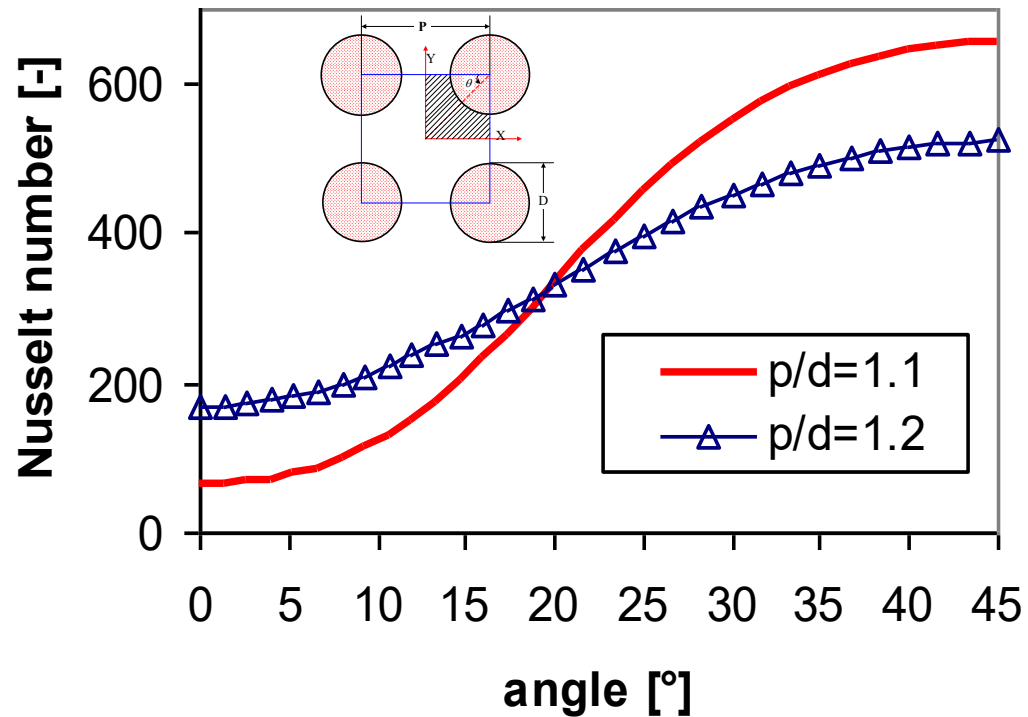
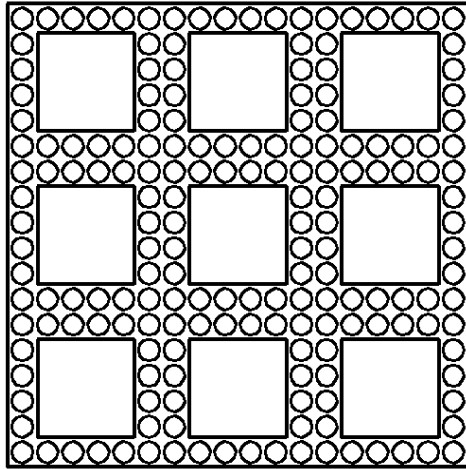
$$\alpha_M$$

Scaling method validation

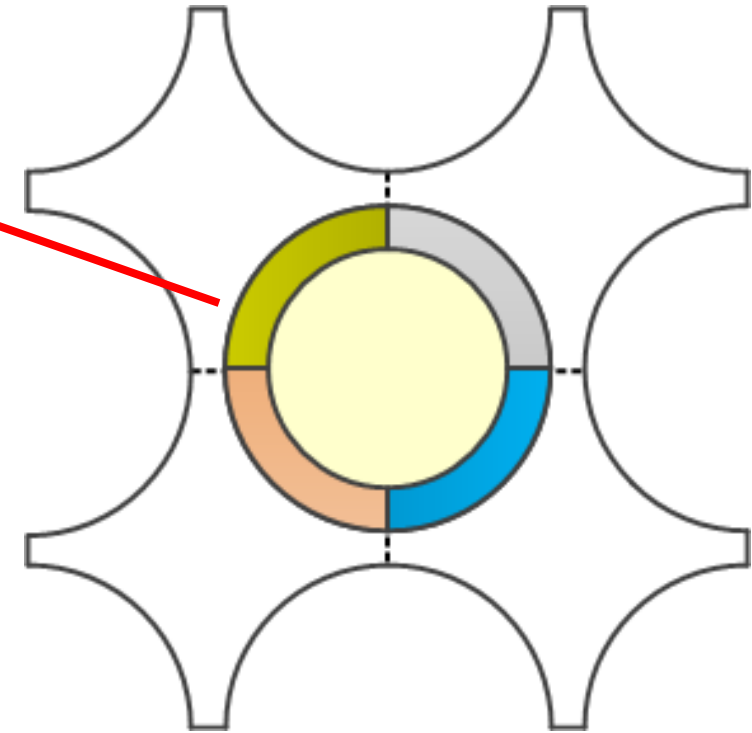
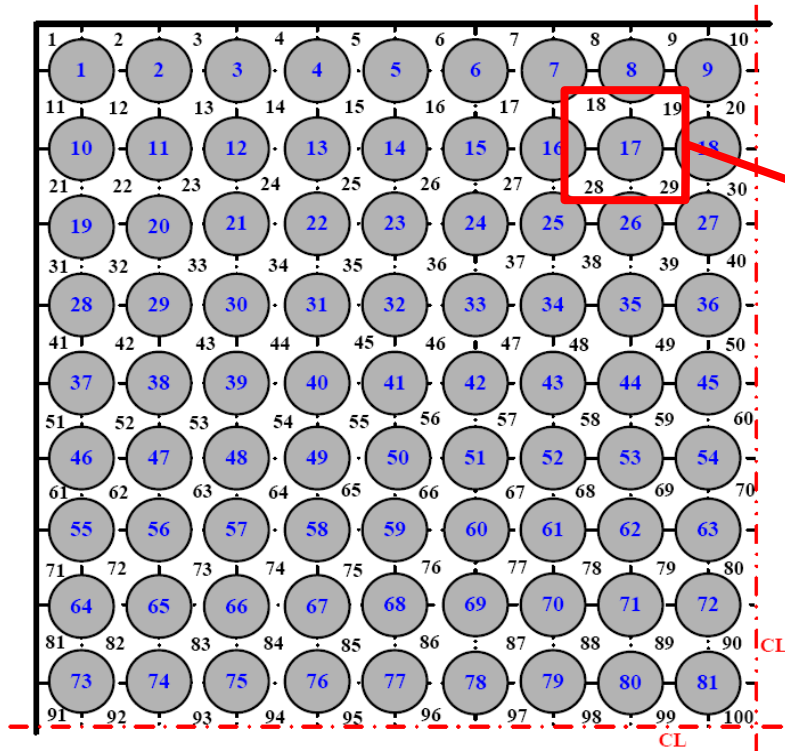


- 76 heat transfer point for R134a,
- Average deviation between the scaled heat transfer coefficient and experimental data is 11%

Supercritical condition: non-uniformity



Supercritical condition: non-uniformity

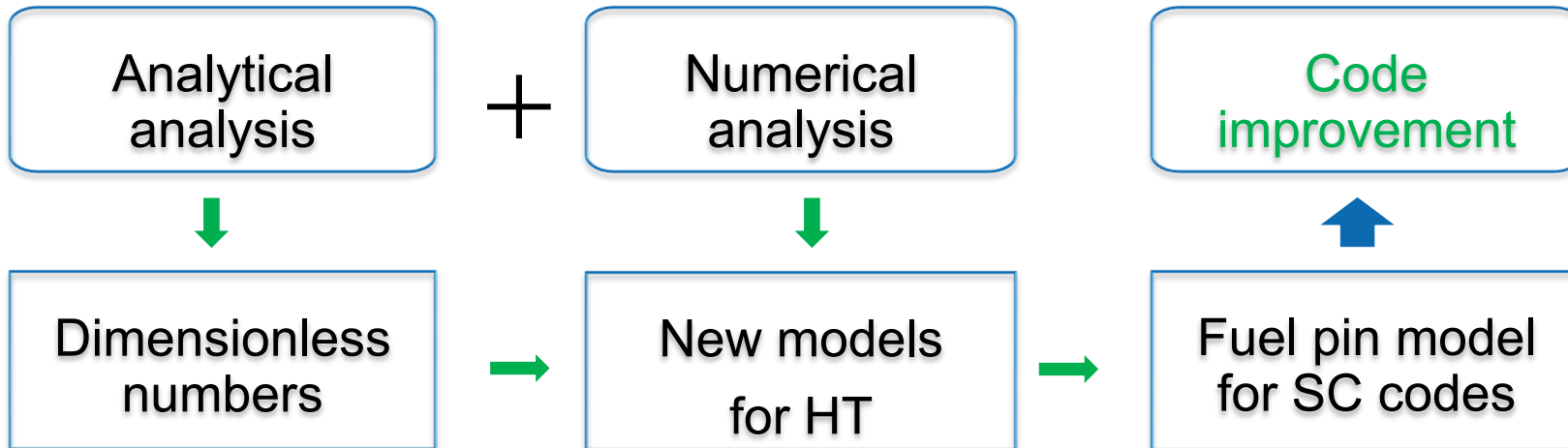


$$T = T(z, r, \varphi)$$

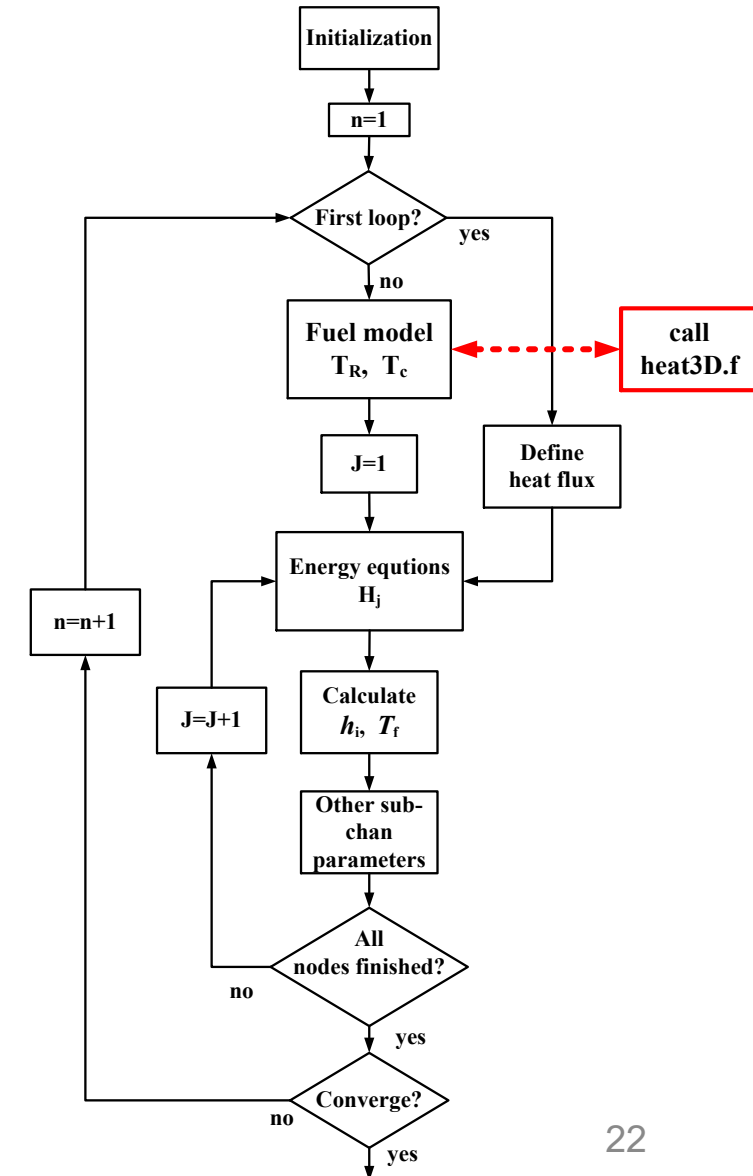
$$\frac{htc_{local}}{htc} = f\left(\varphi, Re, Pr, \frac{p}{d}, \frac{R_{fuel}}{R_{clad}}, \frac{\lambda_{fuel}}{\lambda_{clad}}, \frac{\lambda_{clad}}{\lambda}\right)$$

Supercritical condition: non-uniformity

- Important for tight lattices & blockage
- Limited investigations & no reliable models
- not considered in sub-channel analysis

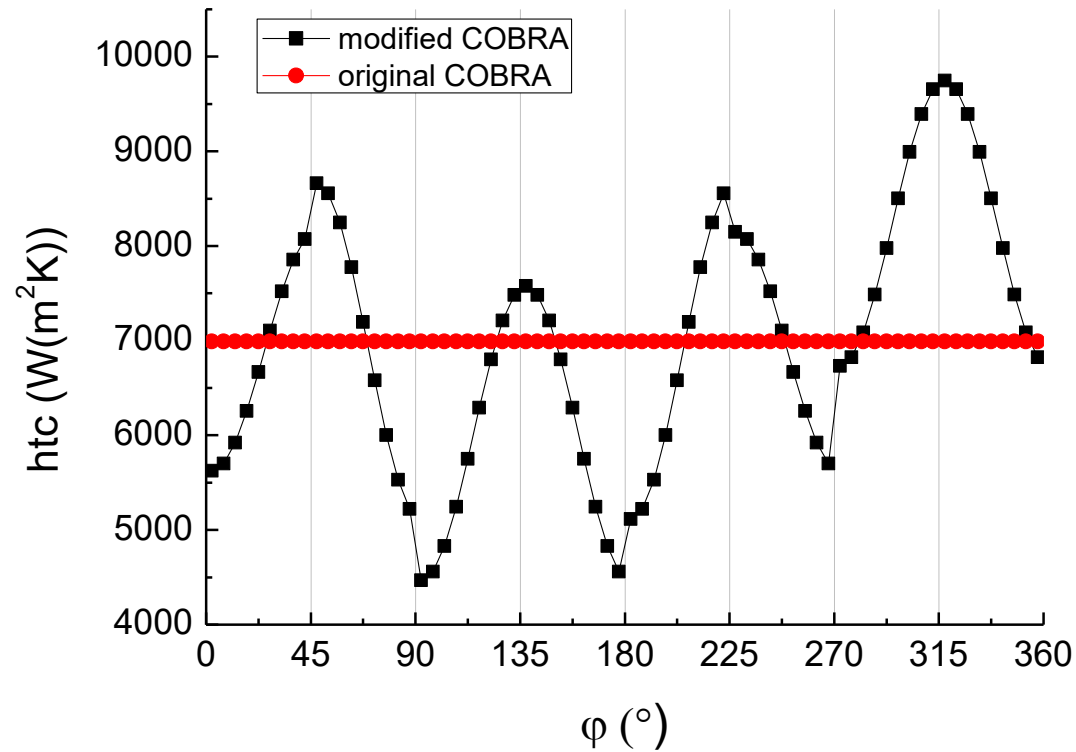
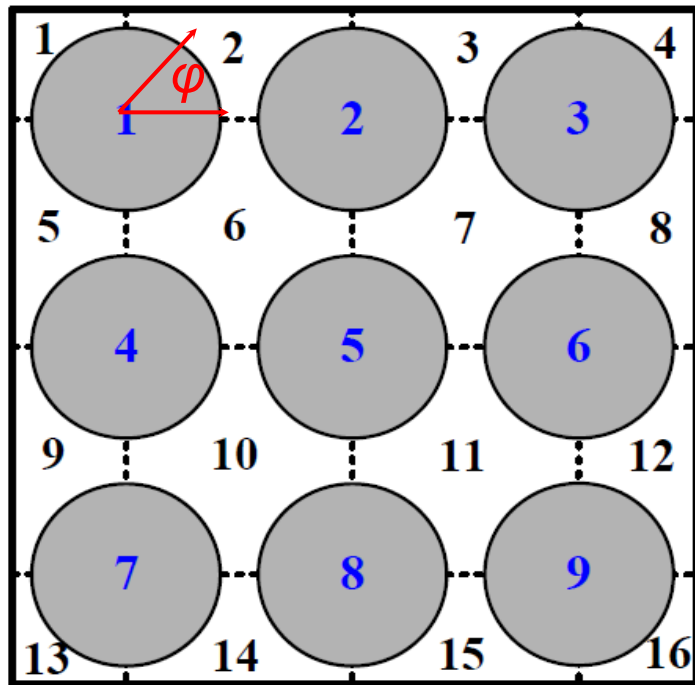


$$htc_N = 1 - \frac{\cos(4\phi)}{1 + 46.8 \left(\frac{p}{d} - 1 \right)^{1.873} Pr^{0.244} \left(\frac{\lambda_{clad}}{\lambda_{coolant}} \right)^{0.229}}$$



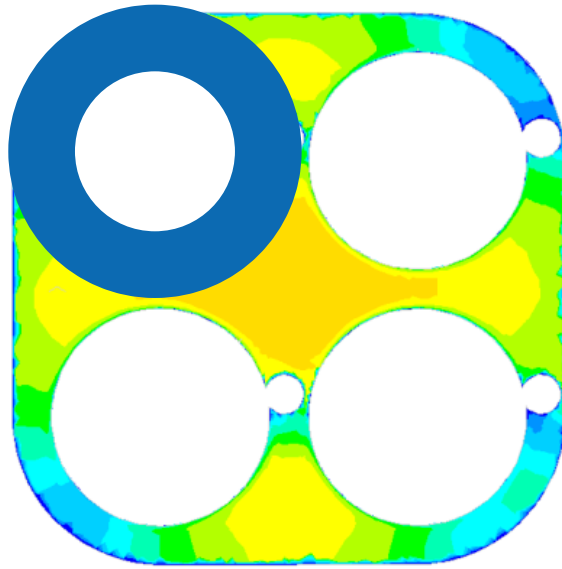
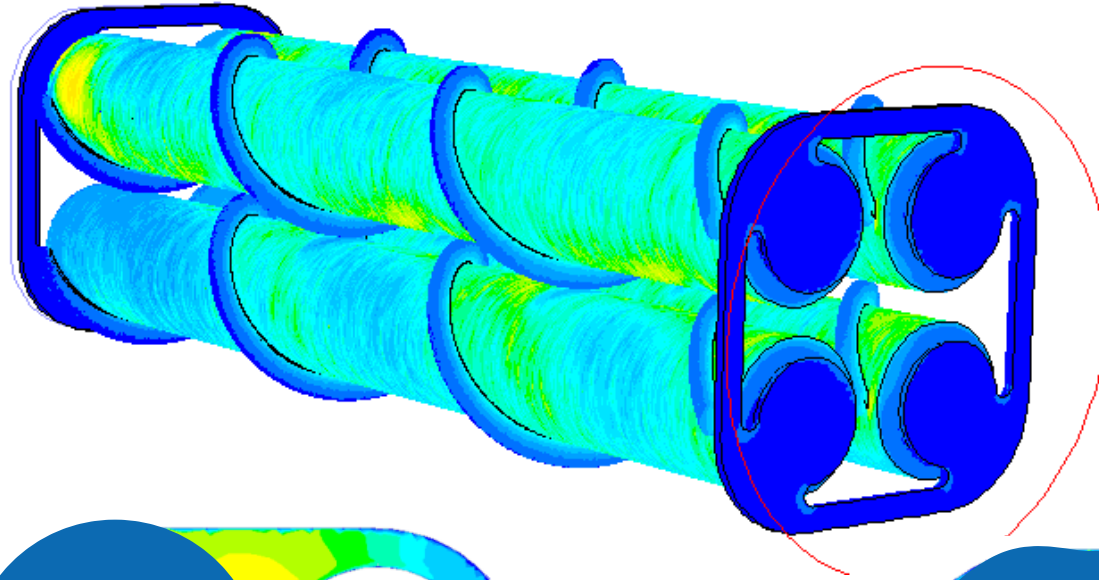
Supercritical condition: non-uniformity

p/d -	elevation m	T_{inlet} °C	p MPa	q'' kW/m ²	G kg/(m ² s)
1.15	1.94	395.0	25.0	454.5	1000

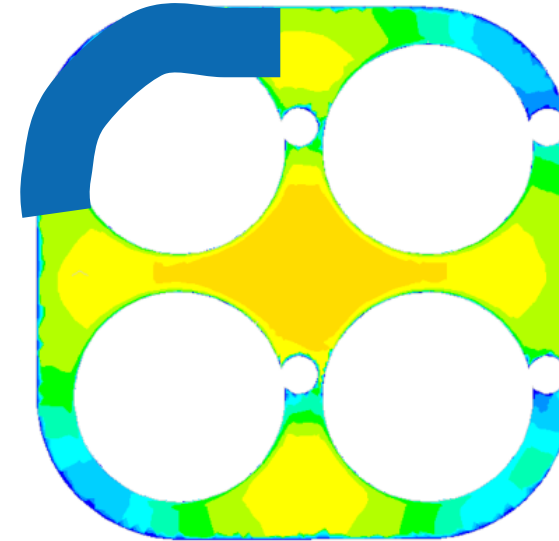


Local htc distribution around Rod 1

Supercritical condition: blockage

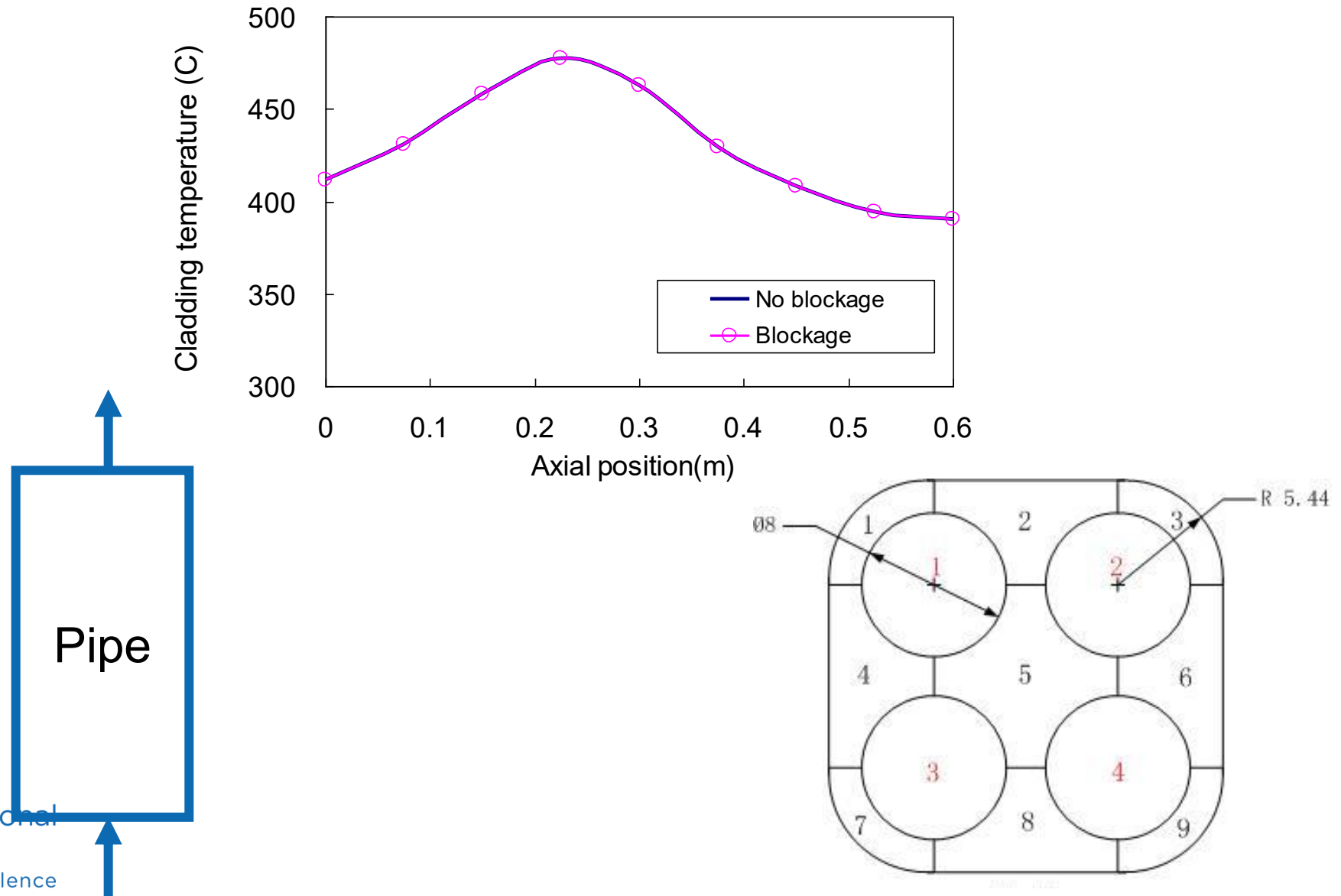


(a) 360 degree blockage of the subchannel around a rod

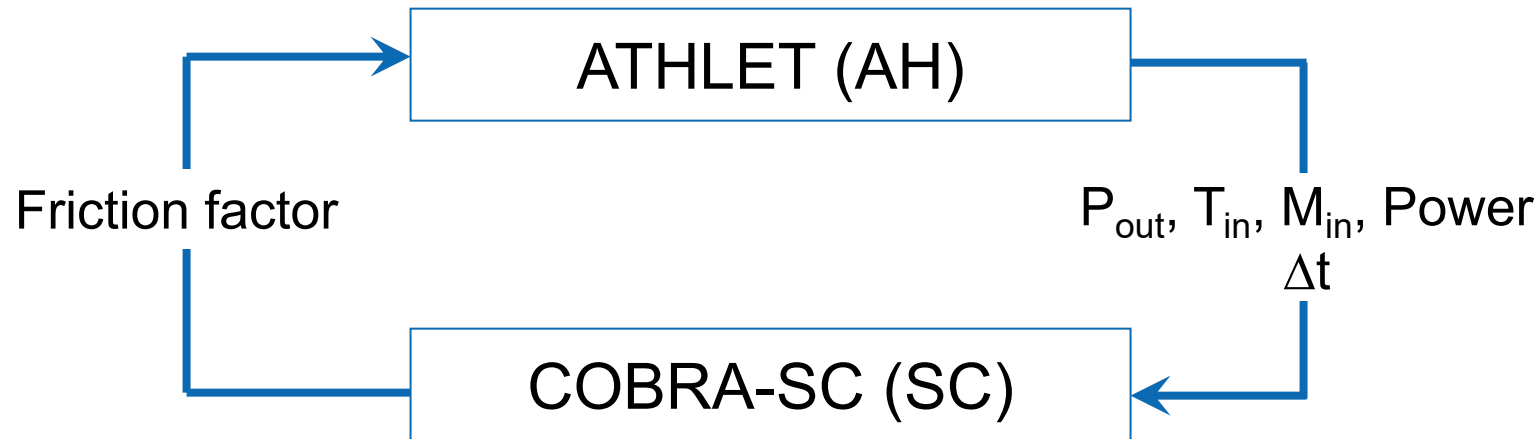


(b) 90 degree blockage of the subchannel around a rod

Supercritical condition: blockage



Supercritical condition: blockage



Common variables

P_{out} = PRESS (outlet-CV)

T_{in} = TDOM (inlet-CV)

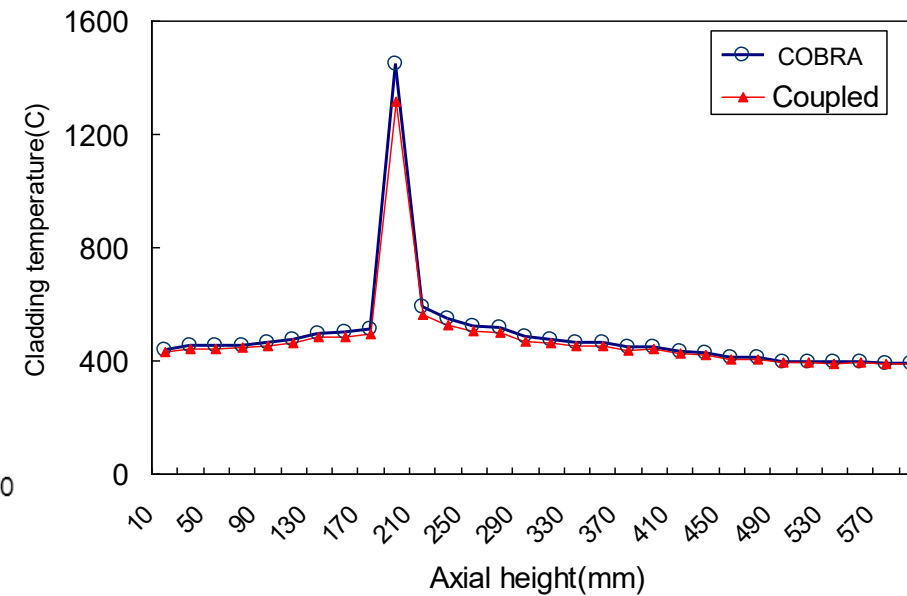
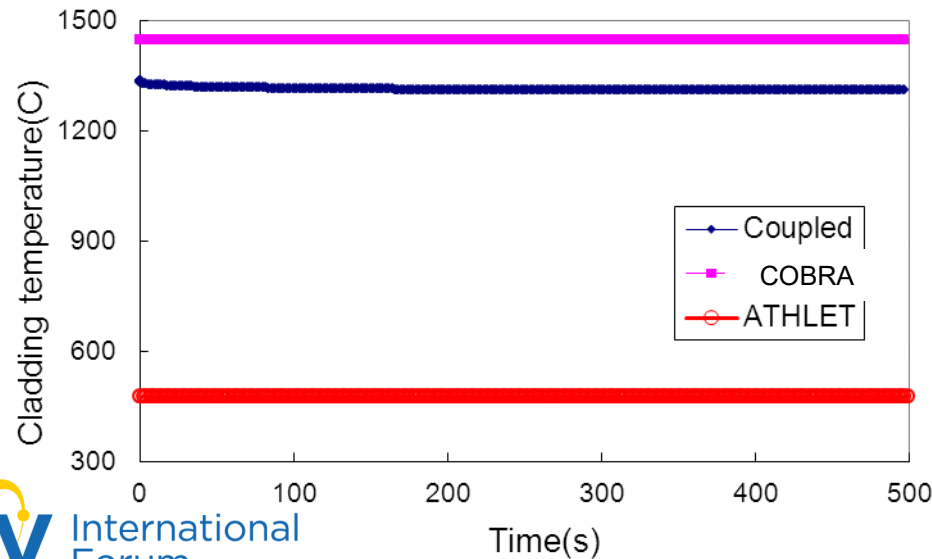
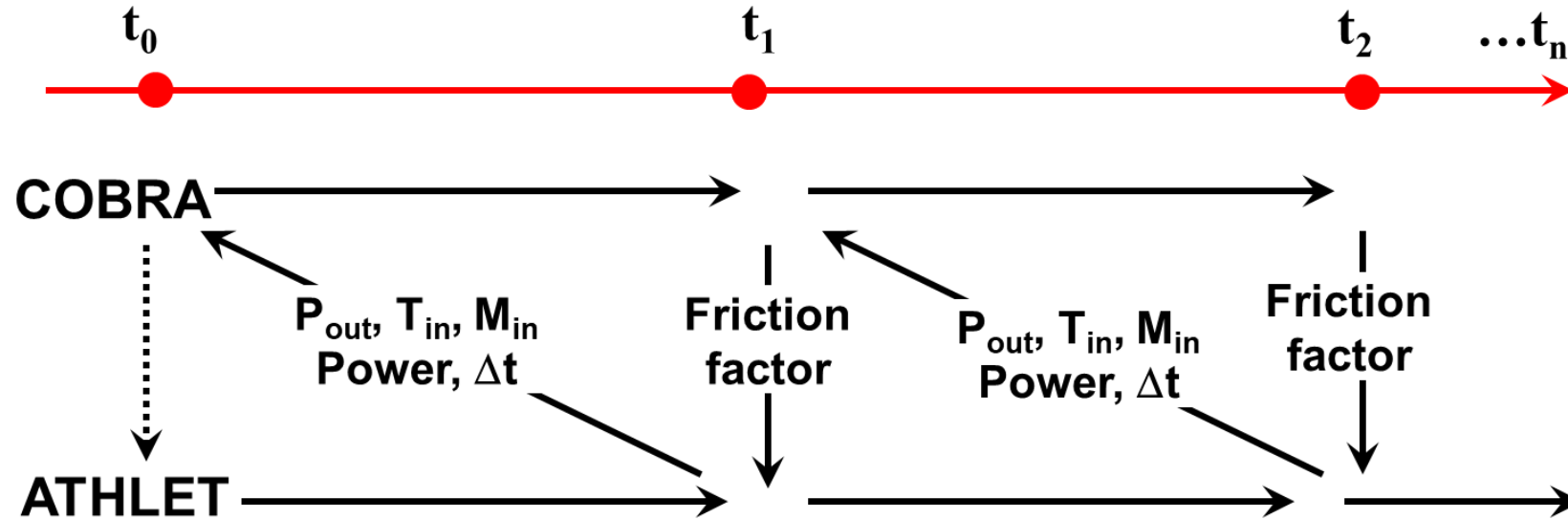
M_{in} = GJ (inlet-junction)

Power = rod power - heat loss from active channel to other channel

Δt = DT

Friction factor: $ALAMO_{(New)} = \Delta P_f(SC) / \Delta P_f(AH) \times ALAMO_{(old)}$

Supercritical condition: blockage

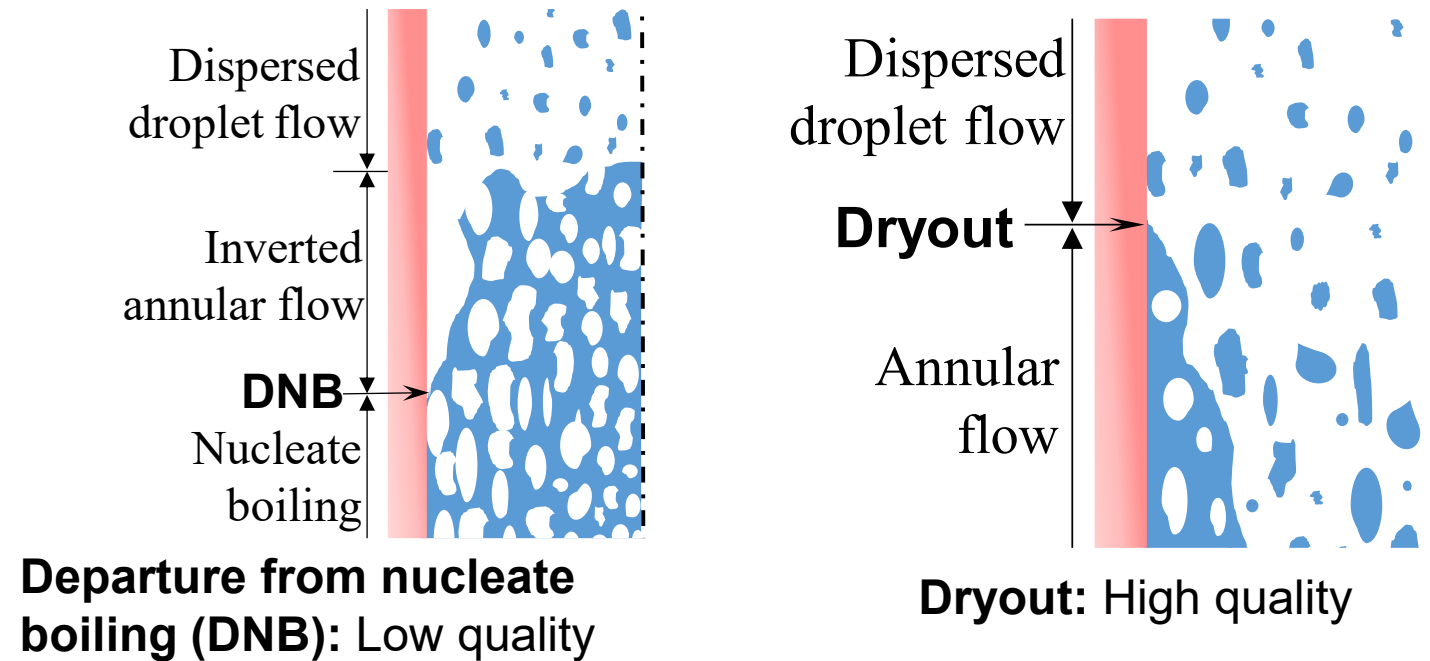


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Subcritical condition

■ Boiling crisis in subcritical condition



Lose continuous liquid contact



Drastic temperature rise



Challenge safety

Subcritical condition- CHF

■ High-pressure CHF experimental databank

■ Water, R12, CO₂

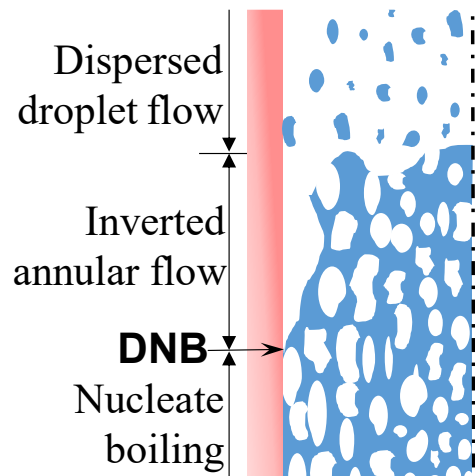
■ Reduced pressure: $P/P_c > 0.7$,

■ 2652 data points, reliable checked

	H ₂ O	R12	CO ₂
P , MPa	15.5 - 21.5	2.9 - 3.5	6.2 - 7.1
G , kg/(m ² ·s)	156 - 6907	121 - 10440	494 - 2041
D_h , mm	1.9 - 24.7	3.0 - 15.8	8.0
x_c , -	-1.768 - 0.955	-0.745 - 0.902	-0.771 - 0.294
q_c , kW/m ²	135.0 - 7770.0	18.0 - 991.0	53.6 - 225.2
No., -	1484	1140	28

Subcritical condition- CHF

DNB: Low quality



■ Sublayer dryout

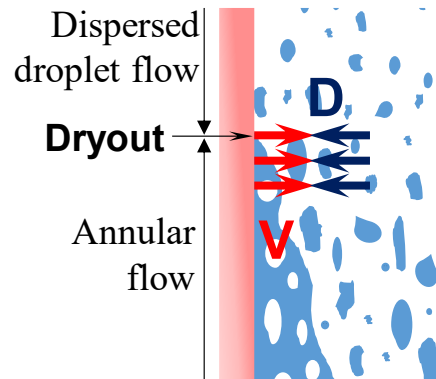
$$q_c = \frac{\rho_L H_{VL} \delta}{L_B / U_B}$$

■ Helmholtz instability

■ Drag force = Buoyancy force

$$\frac{q_c}{GH_{LV}} = f(We_V, Re_L, Pr_L, \pi_D, \pi_\rho, x_c)$$

Dryout: High quality



■ Film dryout

■ Evaporation rate = Deposition rate

■ Work of evaporation force

= Turbulent kinetic energy of droplet

$$\frac{q_c}{GH_{LV}} = f(Re_V, We_V, \pi_\mu, \pi_\rho, x_c)$$

Subcritical condition- CHF

$$\frac{q_c}{GH_{LV}} = f(We_V) \cdot f(x_c)$$

$$f(We_V) = \max(A_1, A_2)$$

$$f(x_c) = (B_1 + B_2 + B_3) - \max(B_1, B_2, B_3) - \min(B_1, B_2, B_3)$$

$$A_1 = 7.796 \times 10^{-2} \cdot We_V^{-0.439}$$

$$A_2 = 1.530 \times 10^{-3} \cdot We_V^{-0.0803}$$

$$B_1 = 2.156 \cdot (1 - x_c)^{0.688}$$

$$B_2 = 1.841 \cdot (1 - x_c)^{2.137}$$

$$B_3 = 0.672 \cdot (1 - x_c)^{0.219}$$

■ Assessment of new CHF correlation with water experiments

Models	ME	RMS	N
Present	0.02	0.374	1484
Miropol'skii	-0.233	0.510	1484
Levitan	0.548	3.223	1484
Chernobai	0.958	2.069	1484
Chen	-0.380	0.706	1254
Becker	-0.952	0.953	1188
Hall	0.133	0.424	414
Lombardi	-0.125	0.881	1188
2006 CHF LUT	0.116	0.537	1387
Katto	0.225	0.891	414
Kariya	0.148	0.960	1484
Vijayarangan	-0.593	0.793	1316
Shah	1.181	2.020	1316

Subcritical condition- CHF

■ Validation of the new CHF correlation with R12 and CO₂

	R12			CO ₂		
Models	ME	RMS	N	ME	RMS	N
Present	-0.020	0.333	1140	0.068	0.304	28
Miropol'skii	-0.807	0.809	1140	-0.805	0.812	28
Hall	-0.162	0.236	356	0.785	0.886	9
Lombardi	-0.349	0.487	1140	-0.607	0.620	28
Katto	0.113	0.319	356	0.002	0.376	9
Kariya	0.434	0.879	1140	0.093	0.304	28
Shah	0.368	1.169	1140	1.277	1.526	28

Subcritical condition- Post-CHF

■ Post-CHF experimental databank

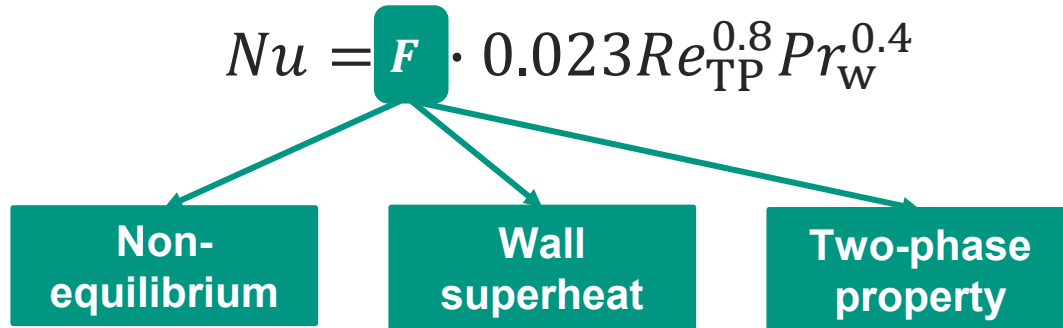
■ Water, R134a, CO₂

■ More than 32 000 data points

	H ₂ O	CO ₂	R134a	H ₂ O (non-uniform)
P , MPa	2.98 - 21.51	6.49 - 7.01	1.10 - 2.82	0.99 - 16.03
G , kg/(m ² ·s)	499.68 - 3500	497 - 1991	294.6 - 1517.4	496.6 - 3117.9
D_h , mm	2.5 - 24.7	8.0	10.0	15.0
q , kW/m ²	147 - 1923	59.8 - 225.2	24.8 - 139.8	70.0 - 1587.0
x_e , -	0.001 - 0.999	0.003 - 0.965	0.263 - 0.999	0.129 - 0.999
$T_w - T_s$, °C	8.66 - 499.68	24.56 - 213.12	30.81 - 190.81	3.74 - 540.82
No., -	9902	497	2806	18895



Subcritical condition- Post-CHF



$$F = F_1 \cdot F_2 \cdot F_3$$

$$F_1 = 8.345824 \times 10^{-3} \cdot Re_{TP}^{0.3186}$$

$$F_2 = \max(0.795 Pr_w^{-1.752}, 0.809 Pr_w^{1.287})$$

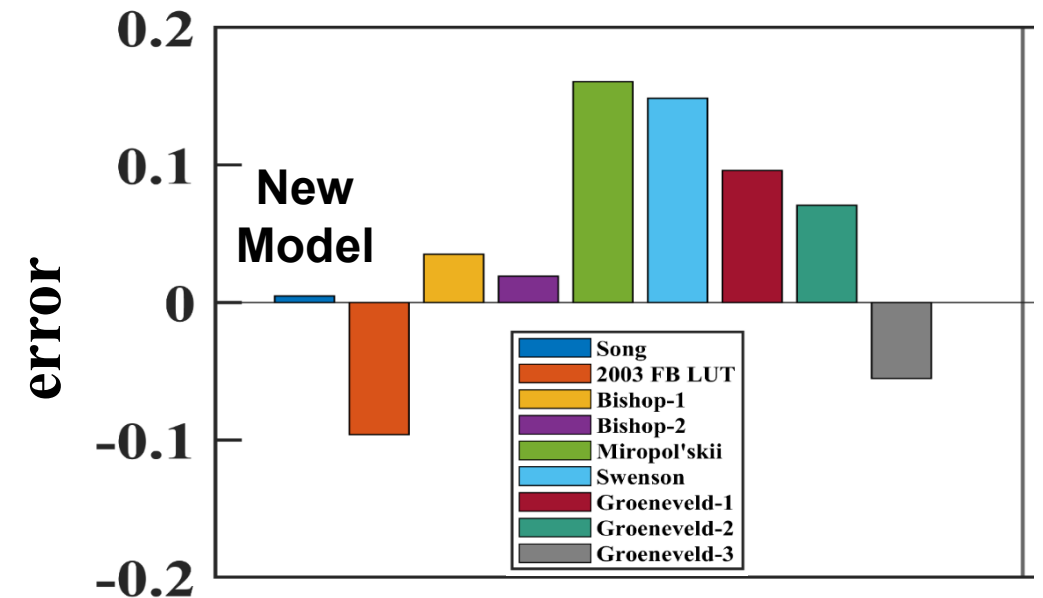
$$F_3 = \min[0.715(1 - x_e)^{-0.678}, 1.0]$$

Model prediction error

H₂O, -1.5%

CO₂, -7.9%

R134a, 2.7%



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Trans-critical transient

■ **ATHLET-SC**

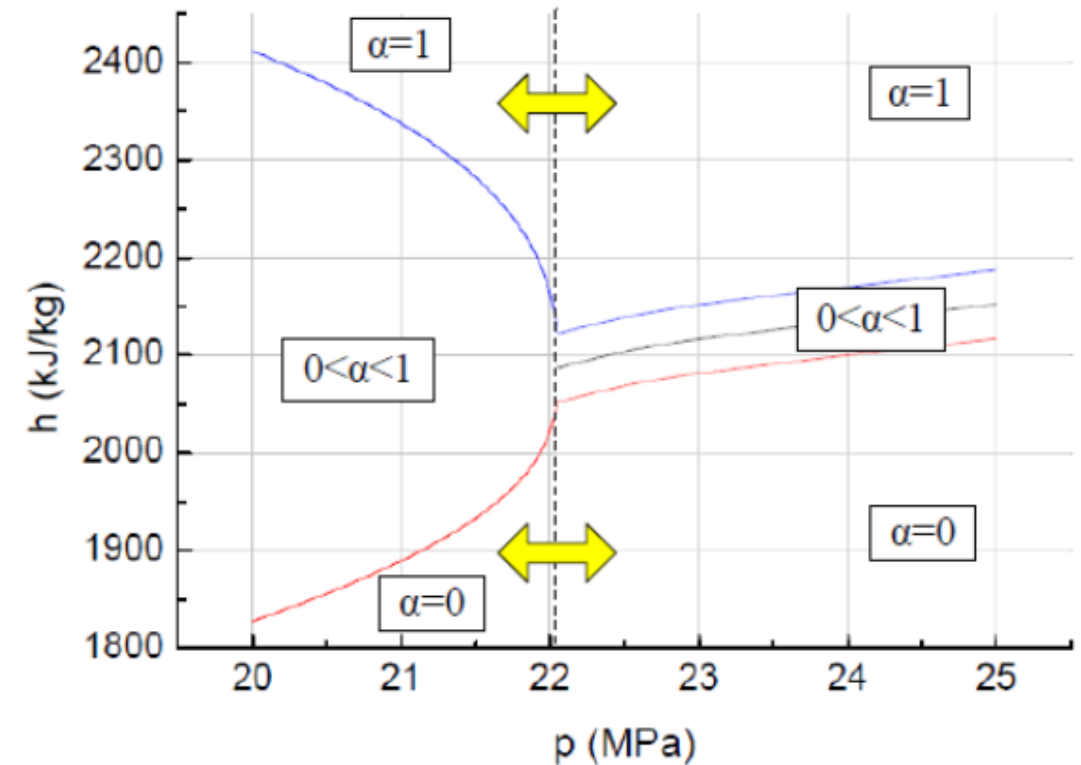
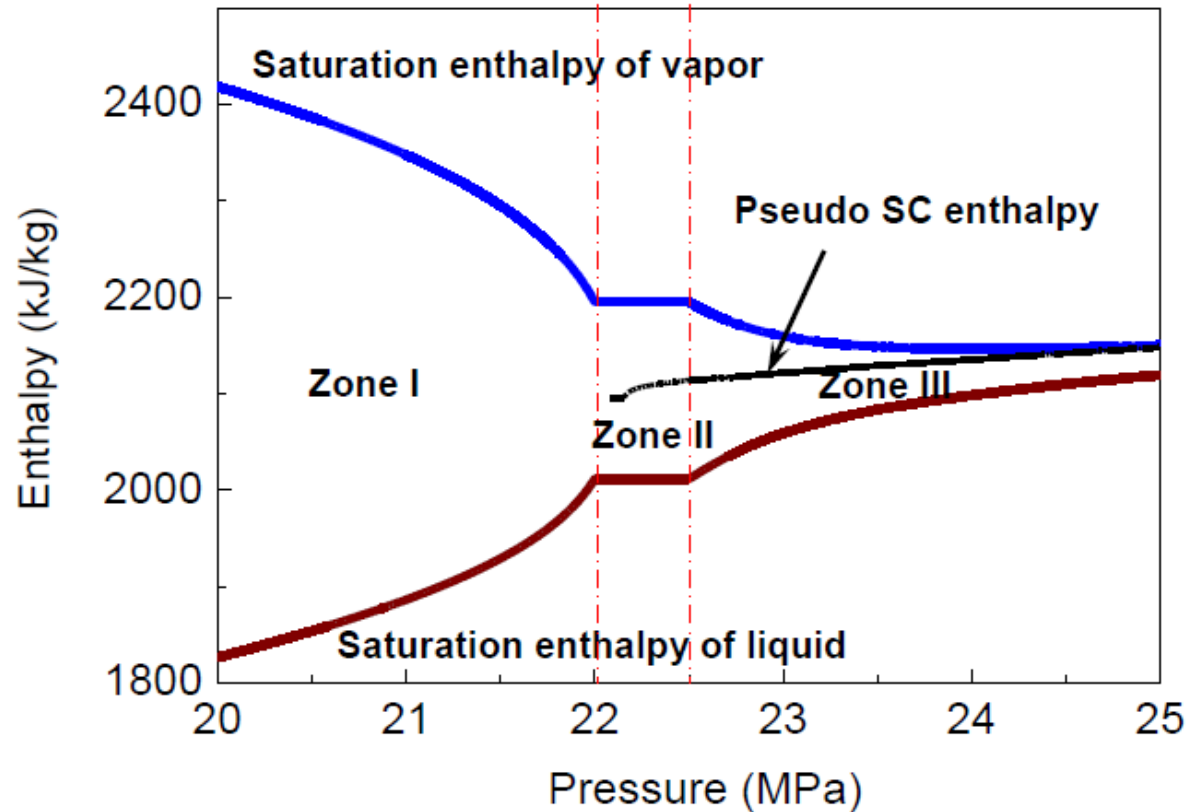
- **System thermal-hydraulic (STH) code**
- **From Gesellschaft für Anlagen- und Reaktorsicherheit (GRS)**
- **Unreliable prediction for trans-critical transient**

■ **Modification of ATHLET-SC**

- ✓ **Supercritical heat transfer correlation**
- ✓ **High-pressure post-CHF heat transfer correlation**
- ✓ **High-pressure CHF model**
- ✓ **Minimum film boiling temperature**

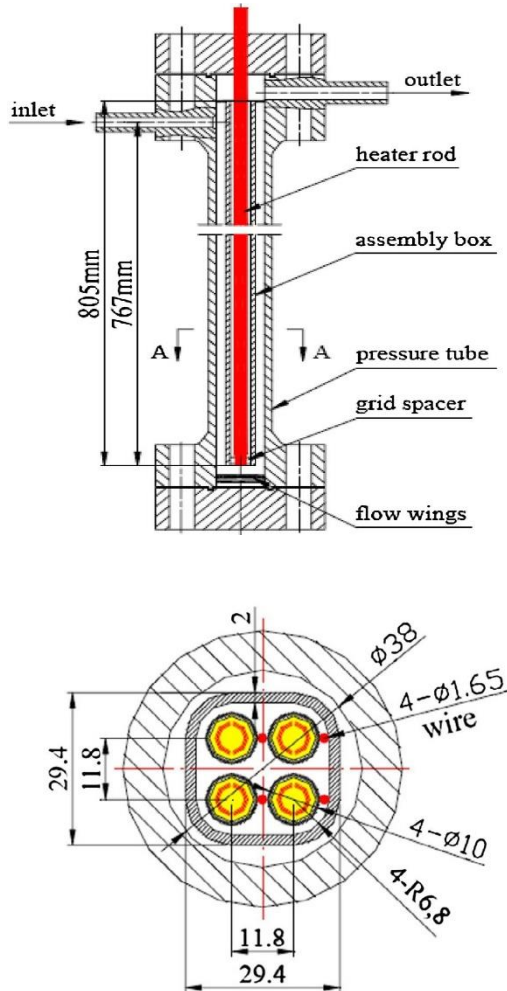
Trans-critical transient

■ Simulation with modified ATHLET-SC



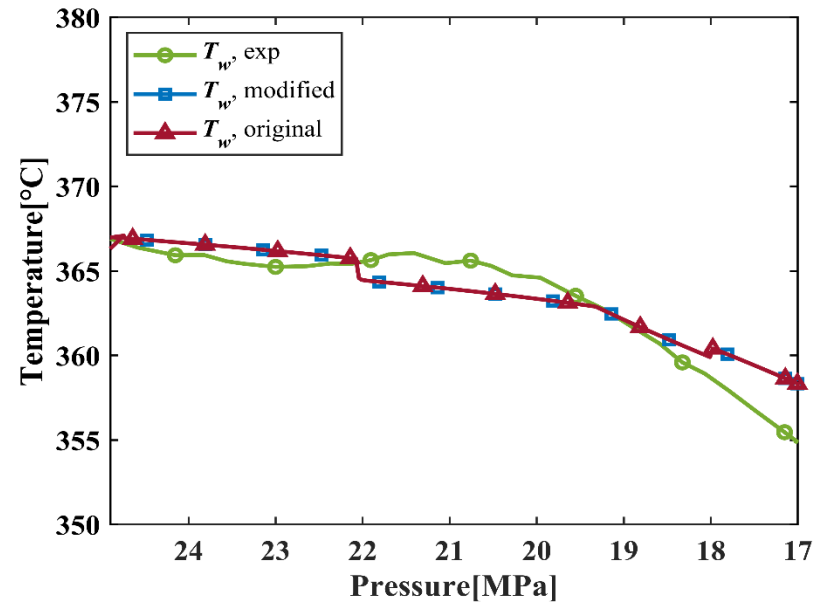
Trans-critical transient

■ Simulation with modified ATHLET-SC



■ Pressure drops from supercritical to subcritical

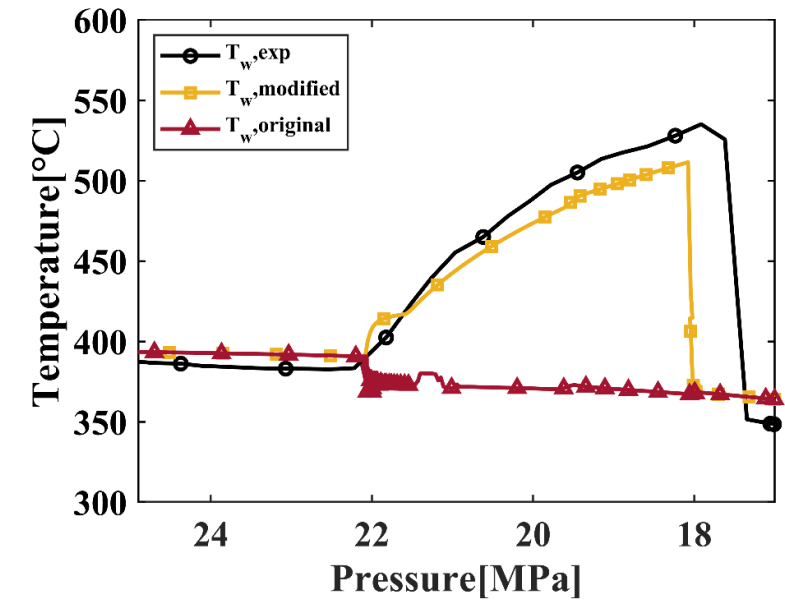
■ Without wall heat up



$$G = 1415 \text{ kg}/(\text{m}^2 \cdot \text{s})$$

$$q = 270 \text{ kW}/\text{m}^2$$

■ With wall heat up

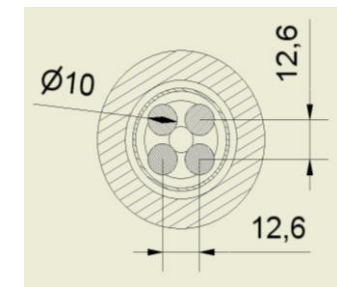
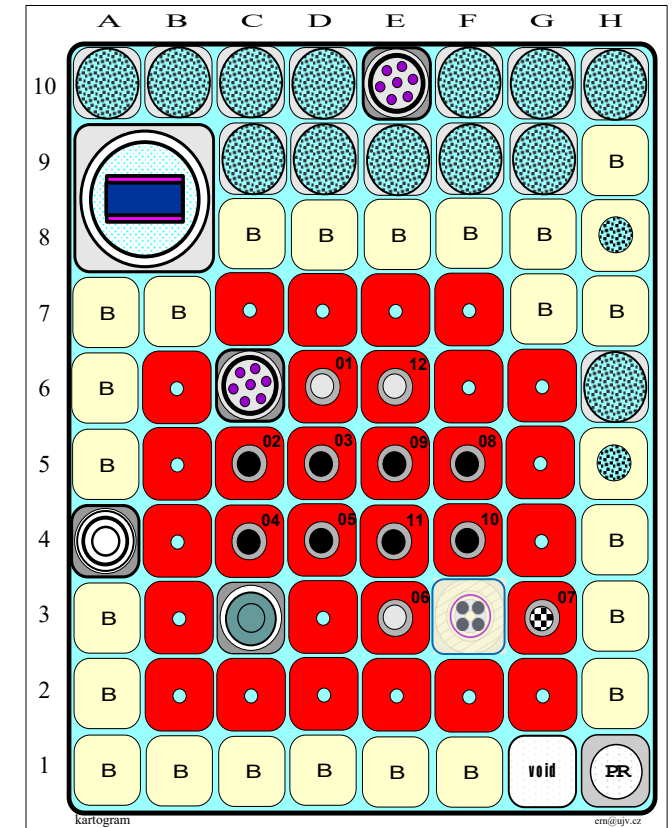
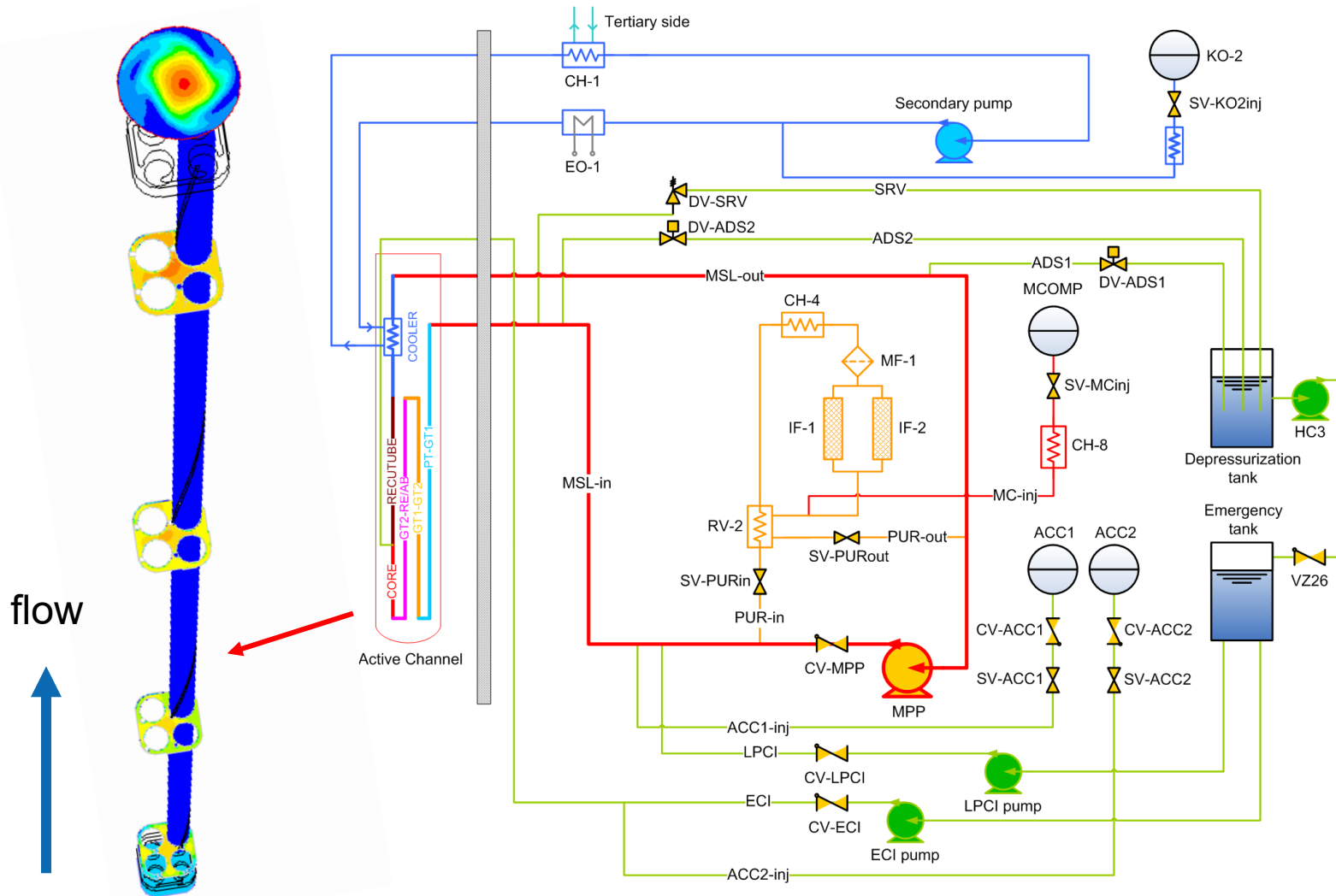


$$G = 1415 \text{ kg}/(\text{m}^2 \cdot \text{s})$$

$$q = 638 \text{ kW}/\text{m}^2$$

Trans-critical transient

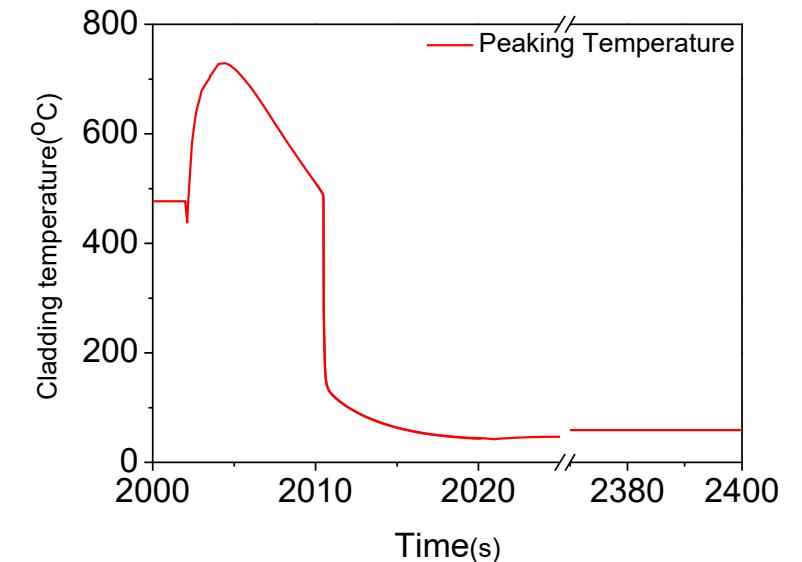
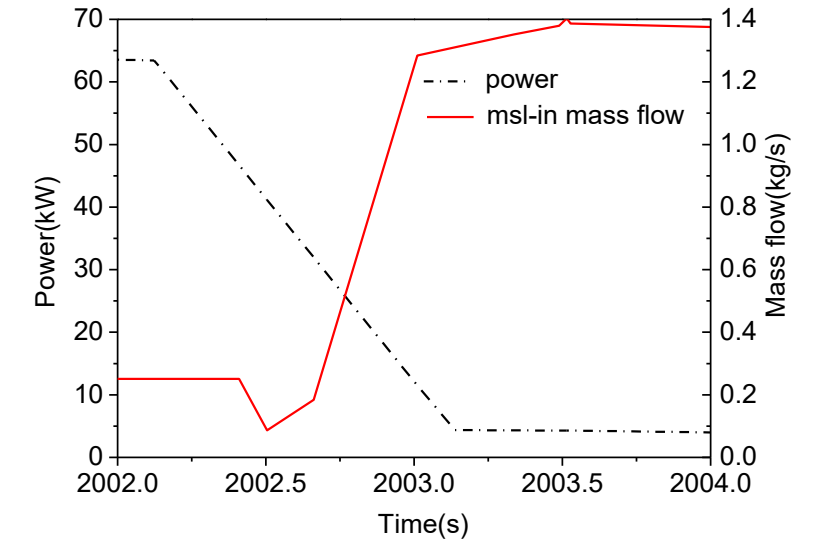
■ Simulation of SCWR-FQT



Trans-critical transient

■ Simulation of SCWR-FQT

Accident	Peaking cladding PCT (°C)
LOCA	
• MSL-out	703
• MSL-in	714
• ECI injection line	752
Trip of the primary pump MPP	685
Coolant bypassing the test section	
• PT-GT1 – COOLER shortcut	1000
• COOLER – ECI shortcut	705
Blockage of the coolant flow path	
• MSL-out	750
• MSL-in	533



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- 2. Heat transfer at Supercritical condition**
- 3. Heat transfer at Subcritical condition**
- 4. Heat transfer during Trans-critical transient**
- 5. Conclusions**

Conclusions

- **Supercritical heat transfer databank and prediction model**
More than 90 000 data points
- **Subcritical databank and prediction model**
CHF: 2652 data points
Post-CHF: More than 32 000 data points
- **Modification of the STH program ATHLET-SC**
Validated by trans-critical experiment
Safety analysis of the SCWR-FQT



上海交通大學

SHANGHAI JIAO TONG UNIVERSITY

谢谢

Thank you!

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Upcoming Webinars

Date	Title	Presenter
24 September 2025	3S interfaces of a pebble-bed small modular advanced reactor	Dr. Bryan van der Ende, Canadian Nuclear Laboratories, Canada
08 October 2025	Science for the safe disposal of nuclear waste – a German perspective	Dr. Francesca Quinto and Dr. Frank Eberling, Karlsruhe Institute of Technology, Germany
05 November 2025	Severe accidents in Sodium Fast Reactors: Safety Study Approach, Prevention and Mitigation by Design	Dr. Frederic Bertrand, Commissariat à l’Energie Atomique et aux Energies Alternatives (CEA), France